

# Mineral Sequestration of Carbon Dioxide in a Sandstone-Shale System

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**Abstract.** A conceptual model of CO<sub>2</sub> injection in bedded sandstone-shale sequences has been developed using hydrogeologic properties and mineral compositions commonly encountered in Gulf Coast sediments. Numerical simulations were performed with the reactive fluid flow and geochemical transport code TOUGHREACT to analyze mass transfer between sandstone and shale layers and CO<sub>2</sub> immobilization through carbonate precipitation. Results indicate that most CO<sub>2</sub> sequestration occurs in the sandstone. The major CO<sub>2</sub> trapping minerals are dawsonite and ankerite. The CO<sub>2</sub> mineral-trapping capacity after 100,000 years reaches about 90 kg per cubic meter of the medium. The CO<sub>2</sub> trapping capacity depends on primary mineral composition. Precipitation of siderite and ankerite requires Fe<sup>+2</sup> supplied mainly by chlorite and some by hematite dissolution and reduction. Precipitation of dawsonite requires Na<sup>+</sup> provided by oligoclase dissolution. The initial abundance of chlorite and oligoclase therefore affects the CO<sub>2</sub> mineral trapping capacity. The sequestration time required depends on the kinetic rate of mineral dissolution and precipitation. Dawsonite reaction kinetics is not well understood, and sensitivity regarding the precipitation rate was examined. The addition of CO<sub>2</sub> as secondary carbonates results in decreased porosity. The leaching of chemical constituents from the interior of the shale causes slightly increased porosity. The limited information currently available for the mineralogy of natural high-pressure CO<sub>2</sub> gas reservoirs is also generally consistent with our simulation. The “numerical experiments” give a detailed understanding of the dynamic evolution of a sandstone-shale geochemical system.

**Key words.** CO<sub>2</sub> sequestration, numerical simulation, mineral trapping, bedded sandstone-shale.

## 1. Introduction

A possible means of reducing carbon dioxide (CO<sub>2</sub>) emissions to the atmosphere is injection of CO<sub>2</sub> into structural reservoirs in deep permeable geologic formations (Holloway, 1997). Such formations could include aquifers, oil and gas fields, and coal seams. Aquifers are the most abundant fluid reservoirs in the subsurface. The deepest aquifers in the United States commonly contain brackish or saline water. Aquifers with salinities exceeding 10,000 mg/L total dissolved solids are excluded by the U.S. Environmental Protection Agency as underground sources of drinking water. Hence, they are logical targets for the eventual disposal of CO<sub>2</sub>. The feasibility of storing CO<sub>2</sub> in aquifers has been discussed in the technical literature over the last decade. These include an evaluation of the feasibility of CO<sub>2</sub> aquifer storage in The Netherlands (Lohuis, 1993) and in the Alberta Basin, Canada (Gunter et al., 1993, Bachu et al., 1994, Perkins and Gunter, 1995; Law and Bachu, 1996, Gunter et al., 1996 and 1997). Furthermore, large-scale CO<sub>2</sub> disposal in an aquifer is already being practiced in the Norwegian sector of the North Sea (Korbol and Kaddour, 1995). Recently, extensive experimental, field, and modeling studies of geological carbon sequestration have been conducted (Pearce et al., 1996; Rochelle et al., 1996; Gunter et al., 1997; Ortoleva et al., 1998; Johnson et al., 2001; White et al., 2001; McPherson and Lichtner, 2001; Oelkers et al., 2002; Rosenbauer, and Koksalan, 2002; Kaszuba, et al., 2002; Boram, et al., 2002; Matter et al., 2002; Giammar et al., 2002; Jones et al., 2002; Goodman, et al., 2002; Hedges et al., 2002; Hovorka, et al, 2002; Horita, J., 2002; Knauss et al., 2002; Solano-Acosta et al., 2002; Palandri and Kharaka, 2002; Strazisar and Zhu, 2002; Perkins et al, 2002; Pruess et al., 2003).

Numerical modeling of geochemical processes is necessary to investigate long-term CO<sub>2</sub> injection in deep aquifers, because aluminosilicate mineral alteration is very slow under ambient deep-aquifer conditions and is not amenable to experimental study. Xu et al. (2004) present a geochemical modeling analysis of the interaction of aqueous solutions under high CO<sub>2</sub> partial pressures with three different rock types. The first rock is a glauconitic sandstone from the Alberta Sedimentary Basin. The second rock type

evaluated is a proxy for a sediment from the United States Gulf Coast. The third rock type is a dunite, an essentially monomineralic rock consisting of olivine.

Xu et al. (2003) performed reactive transport simulations of a 1-D radial well region under CO<sub>2</sub> injection conditions in order to analyze CO<sub>2</sub> immobilization through carbonate precipitation, using Gulf Coast sandstones of the Frio formation of Texas. Most of the simulated mineral alteration pattern is consistent with the observations. Some inconsistencies with field observations are noted. For example, quartz abundance declines over the course of the simulation, while quartz overgrowths are observed during diagenesis due to the release of SiO<sub>2</sub> during replacement of smectite by illite in adjacent shales (Land, 1984). The formation of pyrite in the field is not reproduced by the previous simulation, because sulfur (S) was not included in the kerogen composition.

The previous modeling (Xu et al., 2003 and 2004) was simplified and approximated many of the complexities of actual diagenesis in the field. Major simplifications and limitations include, (1) treating the sandstone aquifer as if it were a closed system isolated from the enclosing shales, and (2) not adequately representing the extremely complex process of kerogen decomposition (or petroleum maturation) in deeply buried sediments. The proportions of reactant minerals in the simulation therefore differ from that of the total system in the field. The long-term interaction of injected carbon dioxide into sandstone aquifers with shale confining layers has not yet been investigated.

Here we present simulation results on mass transfer, mineral alteration, and consequent CO<sub>2</sub> sequestration by carbonate precipitation in a sandstone-shale system. The mineral compositions of sandstone and shale were taken from Gulf Coast sediments. The mineralogy, thermodynamic database and kinetic data are refined from previous studies (Xu et al., 2003 and 2004).

## **2. Numerical Modeling Approach**

### **2.1. Simulation method**

The present simulations were carried out using the non-isothermal reactive geochemical transport code TOUGHREACT (Xu and Pruess, 1998 and 2001). This code was developed by introducing reactive chemistry into the framework of the existing multi-phase fluid and heat flow code TOUGH2 (Pruess et al., 1999). Our modeling of flow and transport in geologic media is based on space discretization by means of integral finite differences (Narasimhan and Witherspoon, 1976). An implicit time-weighting scheme is used for the individual components of the model consisting of flow, transport, and kinetic geochemical reactions. TOUGHREACT uses a sequential iteration approach similar to that of Yeh and Tripathi (1991). After solution of the flow equations, the fluid velocities and phase saturations are used for chemical transport simulation. The chemical transport is solved on a component basis. The resulting concentrations obtained from the transport are substituted into the chemical reaction model. The system of chemical reaction equations is solved on a grid-block basis by Newton-Raphson iteration, similar to those by Parkhurst et al. (1980), Reed (1982), and Wolery (1992). The chemical transport and reactions are iteratively solved until convergence. Full details on the numerical methods are given in Xu and Pruess (1998, 2001).

### **2.2. Process capabilities**

The simulator can be applied to one-, two-, or three-dimensional porous and fractured media with physical and chemical heterogeneity, and can accommodate any number of chemical species present in liquid, gas and solid phases. A wide range of subsurface thermo-physical-chemical processes is considered. The major processes considered for fluid and heat flow are: (1) fluid flow in both liquid and gas phases under pressure and gravity forces, (2) capillary pressure effects for the liquid phase, and (3) heat flow by conduction, convection and diffusion.

Transport of aqueous and gaseous species by advection and molecular diffusion is considered in both liquid and gas phases. Hydrodynamic dispersion is an important solute

transport mechanism that arises from an interplay between non-uniform advection and molecular diffusion. The process is often represented by a Fickian diffusion analog (convection-dispersion equation) that has fundamental flaws and limitations, details on dispersion are discussed in Xu and Pruess (2001). A Fickian model for dispersion is not used in TOUGHREACT. Instead, hydrodynamic dispersion is modeled through appropriate spatial resolution on multiple scales. In any case, the fluid velocity in the present problem is very low.

Aqueous chemical complexation and gas ( $\text{CO}_2$ ) dissolution and exsolution are assumed to be locally at equilibrium. Mineral dissolution and precipitation can be modeled subject to either local equilibrium or kinetic conditions. The kinetic rate law used is given in Section 2.4. The activity of aqueous species is equal to the product of the activity coefficient and molal concentration (mol/kg  $\text{H}_2\text{O}$ ). Aqueous species activity coefficients with the exception of  $\text{CO}_2(\text{aq})$  are calculated from the extended Debye-Hückel equation (Helgeson et al., 1981).  $\text{CO}_2(\text{aq})$  activity coefficient and  $\text{CO}_2(\text{g})$  fugacity coefficient are functions of pressure, temperature and salinity (details on calculations are given in Xu et al., 2004). The so-called “oxygen approach” is used for formulating redox reactions, which relates the oxidation potential to the activity of dissolved oxygen (Nordstrom and Muñoz, 1986; Wolery, 1992).

Changes in porosity and permeability due to mineral dissolution and precipitation can modify fluid flow. This feedback between flow and chemistry can be important and is considered in our model. Changes in porosity during the simulation are calculated from changes in mineral volume fractions. A simple Kozeny-Carman grain model based on spheres was used to calculate changes in permeability due to changes in porosity. The porosity-permeability correlation in geologic media depends on a complex interplay of many factors, such as pore size distribution, pore shapes, and connectivity (Verma and Pruess, 1988). Additional porosity-permeability relationships will be considered in the future. Because diffusion is the main transport process for  $\text{CO}_2$  delivery to the shale from sandstone, the permeability correction is not important for the present simulation.

### 2.3. Thermodynamic data

The quality and accuracy of geochemical modeling is enhanced through the use of internally consistent and critically evaluated thermodynamic data derived from a comprehensive review of the published literature. The primary source for equilibrium constants for aqueous species and minerals used in this study originated with the EQ3/6 V7.2b database (Wolery, 1992). However, many substitutions and changes have been incorporated in response to more recent published revisions in the thermodynamic properties of several rock forming minerals and aqueous species. Among these are revisions to the feldspars by Arnorsson and Stefansson (1999), several clay minerals by Kulik and Aja (1997), and dawsonite (Ferrante et al., 1976). In addition, a comprehensive revision to the properties of silica polymorphs and  $\text{SiO}_2(\text{aq})$  was initiated as a result of a recent refinement by Rimstidt (1997) of the low temperature aqueous solubility of quartz. Revised thermodynamic properties of relevant aqueous species based on the Helgeson-Kirkham-Flowers (HKF) equation of state (Shock et al., 1997), including aluminum species were also incorporated. Changes in the properties of  $\text{SiO}_2(\text{aq})$  and  $\text{AlO}_2^-$  necessitated recomputation of the solubility products for all minerals containing silica or alumina components, whose thermodynamic properties were based on calorimetric measurements.

To ensure consistency with unmodified equilibrium constants in the EQ3/6 V7.2b database, previously generated from thermodynamic data using SUPCRT92 (Johnson et al., 1992), all revised thermodynamic data were incorporated in the SUPCRT92 database and new equilibrium constants similarly generated.

In addition to the changes noted above, the thermodynamic properties of several other phases were estimated and their solubility products incorporated to improve model verisimilitude for this paper. Brief descriptions regarding the methods used to calculate their properties follow.

#### Carbonates

An essential requirement for reactive transport simulations involving  $\text{CO}_2$  sequestration is the need for accurate thermodynamic data of participating carbonate

phases. Recent studies have revealed the possible existence of substantial errors in the Gibbs free energy of formation of magnesite and dolomite (Rock et al., 2001). Furthermore, the experimental consistency of siderite solubility data (Preis and Gamsjager, 2002) has been recently established, and by inference, validated the thermodynamic data for ferrous and ferric ions recommended by Parker and Khodakovskii (1995). These modifications also require a redetermination of the thermodynamic properties of the ankerite solid solution utilized in earlier work (Xu et al., 2004).

The thermodynamic properties of dolomite and magnesite were calculated, using the Gibbs free energy values determined by Rock et al. (2001), together with the respective entropies provided by Robie and Hemingway (1995). These, together with entropy data for end-member ankerite,  $\text{CaFe}(\text{CO}_3)_2$ , from Holland and Powell (1998) and the properties of siderite from Preis and Gamsjager (2002) and calcite from the SUPCRT92 database, were used to calculate the properties of end-member ankerite and the ankerite ideal binary solid solution with the limiting composition:  $\text{CaMg}_{0.3}\text{Fe}_{0.7}(\text{CO}_3)_2$ , using the lattice energy calculations reported by Chai and Navrotsky (1996).

### Chlorite

In prior simulations (Xu et al., 2004), chlorite was represented as a 1:1 mixture of clinochlore and daphnite. The solubility products used were those derived originally from the thermodynamic evaluation of phase equilibria by Helgeson et al. (1978). More recent and more comprehensive evaluations, e.g., that conducted by Holland and Powell (1998) indicate that a revision in the thermodynamic properties of clinochlore and daphnite is called for. Chlorite is only a minor phase in Gulf Coast shales and sandstones. However, chlorite competes with secondary carbonates for magnesium and ferrous iron. Furthermore, the simulation would be more representative if a chlorite solid solution, corresponding to that of ripidolite, were to be included in the reactant minerals of the simulation rather than being represented by a mixture of the end members.

The calculated thermodynamic properties for clinochlore and daphnite were taken from Holland and Powell (1998), and those for chlorite,  $\text{Mg}_{2.5}\text{Fe}_{2.5}\text{Al}_2[\text{Si}_3\text{O}_{10}](\text{OH})_8$ ,

were calculated assuming ideal solid solution between the end members. Thermodynamic properties for both end members of the solid solution were entered into the SUPCRT92 database, retaining the original Maier-Kelly heat capacity function and the ripidolite solubility products recalculated for entry in the TOUGHREACT database.

### Kerogen-OS

Field observations suggest that an important consequence of kerogen maturation is the reduction of ferric iron to ferrous ion (Lynch, 1997) and the formation in small amounts of ubiquitous, secondary pyrite. The sulfur could originate from one or more sources including introduction with connate seawater, the dissolution of distal evaporite beds, biogenic reduction of dissolved sulfate contemporaneous with organic entrapment in accumulating seafloor sediments, or from thiol groups in kerogen itself. The fate of iron in the system during diagenesis is affected by competition between  $\text{HS}^-$  and  $\text{HCO}_3^-$  for the formation respectively of pyrite and ferrous carbonates at elevated  $\text{CO}_2$  partial pressures during  $\text{CO}_2$  sequestration. Preliminary closed system model simulations revealed that the quantity of sulfur would be insufficient were it to be present only in the pore water, and if derived from connate seawater. Furthermore, specified closed-system conditions precluded exogenous introduction through the dissolution of anhydrite or gypsum evaporites, even though this source could be significant in some field scenarios. We therefore refined our representation of kerogen oxygenated functional groups,  $-\text{CHOH}$ ,  $-\text{CHCOOH}$  and  $-\text{CHCOOCH}_2\text{CH}_3$  used in earlier modeling (Xu et al., 2004) through the addition of the thiol group. Although many different cross-linking sulfur-sulfur and sulfur-carbon bonds have been identified in type II kerogen, (e.g. see Hold et al., 1998), we decided, for simplicity, to incorporate sulfur simply as  $-\text{CHSH}$ . The sulfur was incorporated in the molar ratio  $\text{O}:\text{S}::4:1$ , which is approximately equivalent to the average ratio found in Type II kerogen analyses summarized by Tissot and Welte (1978, Table II.4.1). Thus the final composition of the kerogen functional groups, designated Kerogen-OS is  $-(\text{CHOH})_{18}(-\text{CHCOOH})_5(-\text{CHCOOCH}_2\text{CH}_3)_6(-\text{CHSH})_{10}$ .

In computing the thermodynamic properties of the attached oxygenated functional groups, the molal properties ( $\Delta G_f^\circ$ ,  $\Delta H_f^\circ$ ,  $S^\circ$ , and the Maier-Kelley heat capacity function coefficients,  $a$ ,  $b$ ,  $c$ ) of functional group components were taken from Helgeson et al.



(1998) and Richard and Helgeson (1998). The thermodynamic properties of –CHSH were calculated assuming that the difference between –CHOH and –CHSH was the same as the difference between liquid methanol, CH<sub>3</sub>OH and liquid methanethiol, CH<sub>3</sub>SH. Relevant data for methanethiol were taken from Russell et al. (1942) and Good et al. (1961), as summarized by NIST (<http://webbook.nist.gov>). For methanol, data were taken from Baroody and Carpenter (1970), Carlson and Westrum (1971), and for C<sub>p</sub>, an average of 13 values given by NIST, (loc. cit.) from references between 1981 and 1992. Molar volume differences were calculated from density data given in the Handbook of Physical Chemistry. The computed thermodynamic properties of the oxygenated functional groups and –CHSH were summed and appropriate dissociation equilibria for kerogen-OS calculated using SUPCRT92 (Johnson et al., 1992).

#### Revision of Fe<sup>2+</sup> and Fe<sup>3+</sup>

Uncertainties relating to the thermodynamic properties of the ferrous and ferric ions in aqueous solution have bedeviled precise modeling of geochemical systems involving these species for some time, e.g. see Nordstrom (1984) and Reardon and Beckie (1987). Recent work on the solubility of siderite (Preis and Gamsjager, 2002) provides support for the validity of the properties of Fe<sup>2+</sup> in the survey by Parker and Khodakovskii (1995). We therefore incorporated revised properties of Fe<sup>2+</sup> and Fe<sup>3+</sup> in SUPCRT92 and recalculated the solubility products of all participating iron-containing minerals whose thermodynamic properties were derived from calorimetry. These included chlorite, daphnite, pyrite, and hematite, as well as appropriate corrections to the solubility products of siderite and ankerite.

#### **2.4. Kinetic data**

For kinetically-controlled mineral dissolution and precipitation, a general form of rate law (Lasaga, 1984; and Steefel and Lasaga, 1994) is used

$$r_m = \pm k_m A_m a_{H^+}^n \left[ \left( \frac{Q_m}{K_m} \right)^\mu - 1 \right]^v \quad (1)$$

where  $m$  is mineral index,  $r_m$  is the dissolution/precipitation rate (positive values indicate dissolution, and negative values precipitation),  $A_m$  is the specific reactive surface area per kg  $H_2O$ ,  $k_m$  is the rate constant (moles per unit mineral surface area and unit time) which is temperature dependent,  $a_{H^+}$  is the activity of  $H^+$  and  $n$  is empirical reaction order accounting for catalysis by  $H^+$  in solution.  $K_m$  is the equilibrium constant for the mineral-water reaction written for the destruction of one mole of mineral  $m$ ,  $Q_m$  is the reaction quotient, the parameters  $\mu$  and  $\nu$  are two positive numbers normally determined by experiment, and are usually, but not always, taken equal to unity (as in the present work). The temperature dependence of the reaction rate constant can be expressed reasonably well via an Arrhenius equation (Lasaga, 1984; and Steefel and Lasaga, 1994). Since many rate constants are reported at 25 °C (298.15 K), it is convenient to approximate rate constant dependency as a function of temperature, thus

$$k = k_{25} \exp \left[ \frac{-E_a}{R} \left( \frac{1}{T} - \frac{1}{298.15} \right) \right] \quad (2)$$

where  $E_a$  is the activation energy,  $k_{25}$  is the rate constant at 25 °C,  $R$  is gas constant, and  $T$  is absolute temperature.

Mineral dissolution and precipitation rates are a product of the kinetic rate constant and reactive surface area (Eq. 1). The parameters used for the kinetic rate expression are given in Table 1. Calcite is assumed to react at equilibrium because its reaction rate is typically quite rapid. In Table 1, we include the separate rate constant ( $k_{25}$ ), the activation energy ( $E_a$ ), and the reaction order ( $n$ ) for each mechanism (acid catalyzed and no catalysis). At any pH the total rate is the sum of the rates via each mechanism. The acid catalysis is considered only for mineral dissolution. The temperature-dependent kinetic rate constants are calculated from Eq. 2. Some kinetic parameters were taken directly from the published scientific literature. The references are listed in the fifth column of Table 1. Others were set to the minerals with known kinetic properties. The evolution of surface area in natural geologic media is very complex,

especially for multi-mineralic systems, and is not quantitatively understood at present. Mineral reactive surface areas (last column of Table 1) were taken from Sonnenthal and Spycher (2001), which were calculated assuming a cubic array of truncated spheres that make up the framework of the rock. For clay minerals kaolinite, illite, and smectite, surface areas were increased to account for edges in these sheet silicate minerals (Nagy, 1995). The kinetic rate constants given in Table 1 were normalized to BET surface areas in the original studies. The geometric surface areas should be normalized to BET surface areas according to the roughness factor of individual minerals. A reactive surface area calculated from grain size may be a poor estimate of the hydrologically accessible mineral surface area. Furthermore, in multi-mineralic field scale systems the reactive surface area for a given mineral is generally smaller due to many factors such as coating. To account these effects, surface areas listed in Table 1 were arbitrarily reduced by one order of magnitude in the present simulations.

The precipitation of possible secondary minerals is represented using the same kinetic expression as that for dissolution. However, several aspects regarding precipitation are different from dissolution, including nucleation, crystal growth and Ostwald ripening processes, as well as the calculation of the reactive surface area (Steefel and van Capellen, 1990). These processes for mineral precipitation are not considered in the current model. The magnitudes of surface areas are highly uncertain and cover a wide range of values. Sensitivity regarding the kinetic rate constants and reactive surface areas are addressed later in this paper.

### **3. Problem Setup**

#### **3.1. Sandstone-shale configuration and properties**

Much specific and detailed information will be required to assess the feasibility of disposing of CO<sub>2</sub> in a sandstone-shale formation at any particular site, and to develop engineering designs for CO<sub>2</sub> disposal systems. Before moving into site-specific investigations, general features and issues relating to the formation injection of CO<sub>2</sub> should be explored. This can be done by investigating a sandstone-shale system that

abstracts site-specific features representing characteristics that are common to many such systems.

A basic issue is the mass transfer and geochemical behavior in bedded sandstone-shale sequences under high-CO<sub>2</sub> pressure conditions. A simplified 1-D model of a sandstone-shale system is used (Figure 1). Hydrological parameter specifications for sandstone and shale layers were chosen to represent conditions encountered in Texas Gulf Coast sediments at a depth of order 2 km (Table 2). A porosity of 0.3 was used for sandstone based on Loucks et al. (1984), and a porosity of 0.1 for shale based on Howard (1991). Porosity may vary from sample to sample. Nevertheless, variations of porosity do not affect the mineral alteration pattern. The model grid is made finer in the shale near the interface between sandstone and shale to better resolve concentration gradients in the low permeability shale. Only one grid block was used for the sandstone layer and the calculation point for this block was placed at the interface. This represents a conceptual model of perfect mixing throughout the sand.

### **3.2. Mineralogy and geochemistry**

A proxy for sandstone-shale sequences from the United States Gulf Coast was used to represent the mineralogy and geochemistry. The initial mineral composition of sandstone used in the present modeling (Table 2), was taken from Xu et al. (2004). The specification of formation mineralogy is determined in part by the availability of data. Most studies related to the Tertiary Gulf Coast sediments are concentrated in the state of Texas. The principal reservoir-quality sandstones within that region are found in the Frio, the Vicksburg and the Wilcox formations, all of which are Lower Tertiary age. Of the three formations, the Frio was chosen as a representative candidate for the sequestration of supercritical CO<sub>2</sub>. It is the shallowest of the three formations, but over much of its areal extent, it is located at depths between 1,524 and 6,096 m, sufficient to ensure adequate CO<sub>2</sub> densities for effective storage.

Loucks et al. (1984) used the sandstone classification of Folk (1968) to describe sandstone reservoirs in the Lower Tertiary Gulf Coast sediments of Texas. This classification projects the composition of sandstones onto a ternary diagram in terms of the components: quartz, feldspar and rock fragments. For the purposes of this study, the

approximate mean composition of the Frio sandstone in the middle Texas region of the Gulf Coast was chosen. This composition is a representative of a quartzose lithic arkose with 56% quartz, 28% feldspar and 16% lithic fragments. According to Loucks et al. (loc. cit.), the lithic fragments in the Frio formation of this region are predominantly volcanic fragments, although significant percentages of metamorphic rocks are present. Carbonate rock fragments are also present in minor amounts. The volcanic fragments are believed to be mainly rhyolites and trachytes, which have been silicified or altered to chlorite. The carbonate fragments were apparently locally derived from adjacent landmass caliche soils. Neither the provenance nor the character of the metamorphic rocks is described.

The fractions of plagioclases and alkali feldspars making up the feldspar component, and the mineralogy of the lithic fragments are based on the work of Land (1984), who reports 1,634 electron probe point counts on 29 Frio formation rocks. About 30% of the original feldspar was K-feldspar and the remainder was plagioclase having an average anorthite (An) content of 20%. The composition of the lithic fragments has been described only qualitatively, and therefore, the actual mineral composition can only be surmised. Secondary minerals (calcite, clay minerals, and iron oxides) are not included in published lithological classifications. Therefore, the inclusion of these phases is based on subjective estimates. The observed presence of chlorite in lithic fragments of volcanic rock (Loucks et al., loc. cit.) is represented by 4.6 vol.% ripidolite. A small amount of hematite (0.5 vol.%) was added to take into account the presence of ferric iron staining. The concentrations of clay minerals, smectite, illite and kaolinite were arbitrarily assigned concentrations of 3.9, 1.0 and 2.0 vol.% respectively, and assigned as the residue of the mineral contribution by lithic fragments. The compositions of smectite and illite are those representative of I/S clays, typical of Gulf Coast sediments.

The model shale composition is based on the recent study by Land et al. (1997) of Upper Oligocene - Lower Miocene mudrocks obtained at depths between 2130 and 5490 m from the Mobil #406 State Tract well in Kenedy County, Texas. Neither the location, nor the provenance of the studied mudrocks corresponds closely with the selected model sandstone. The Mobil #406 State Tract well is located on the South Texas Gulf Coast whereas the sandstone composition was selected as representative of the mid Texas Gulf

coast (Loucks et al., 1984). However, the quality of the analytical and mineralogical analyses is believed to be superior to earlier, but potentially more representative analyses such as those by Hower et al. (1976), for the reasons cited by Land et al. (loc. cit.), and therefore are preferred.

The mineralogical analyses given in Table 1 of Land et al. (1997) were plotted versus depth, and linearly regressed to obtain a functional relation with depth. Not all trends were linear, and slightly better fits were obtained in some cases with second order polynomial equations despite the substantial scatter in the data. However, only the linear correlations were used, and these were extrapolated incrementally to a depth of 2,000 m, corresponding to an approximate ambient temperature of approximately 75 °C. The mineralogical concentrations (Wt.%) were converted to specific volumes ( $\text{m}^3/\text{mol}$ ) and normalized to 98 vol.%, the balance of 2 vol.% being assigned to organic matter, i.e. kerogen-OS. In the process of making these calculations, some simplifications and assumptions were introduced to facilitate modeling. All plagioclase was assumed to have the composition of oligoclase (Table 3), chlorite was assumed to have a 1:1 clinocllore:daphnite composition, corresponding to ripidolite. Finally, the I/S was divided into separate illite and smectite components in accordance with the mineralogical compositions for I/S specified by Kulik and Aja (1997), and the illite component lumped with the detrital illite. The smectite component is assumed to be a sodium end member, as would be expected if in contact with a 1-molal solution of NaCl. These adjustments are considered realistic compromises in the light of current model development. The resulting mineralogical composition of the shale is presented in Table 3.

Prior to the reactive transport simulations in the sandstone-shale system, batch geochemical modeling of water-rock interaction for individual sandstone and shale was performed to obtain a nearly equilibrated water chemistry (see Table 4) using a pure 1.0 M solution of sodium chloride and  $\text{CO}_2$  gas pressure ( $P_{\text{CO}_2}$ ) of  $1 \times 10^{-2}$  bar reacting with the primary minerals listed in Table 3 at a temperature of 75 °C. We chose  $P_{\text{CO}_2} = 10^{-2}$  bar at 75°C, to ensure that the pH of the pore water fell into the general range observed for Gulf Coast brines with a salinity of about 1.0 mol/L, e.g. see Kreitler and Richter (1986), rather than specifically attempting to replicate  $P_{\text{CO}_2}$ . The resulting water chemistry (Table 4) was used for the initial condition of reactive geochemical transport simulations.

A separate supercritical CO<sub>2</sub> phase (called gas phase in this paper) is initially placed in the sandstone grid block with a gas phase saturation of 0.5 and a water saturation of 0.5. Whereas, the shale layer is initially water saturated. A CO<sub>2</sub> gas pressure of 201 bars is used in the simulation, which is close to hydrostatic pressure at a depth of 2 km. A temperature of 75°C is used based on a land surface temperature of 15°C and a geothermal gradient of 30°C/km. The CO<sub>2</sub> gas phase is assumed to be in equilibrium with the aqueous phase at all times. The solubility of CO<sub>2</sub> in the aqueous phase depends on pressure, temperature, and salinity. The details on solubility calculations are given in Xu et al. (2004). The reactive geochemical transport simulations were performed for a period of 100,000 years.

The first simulation used parameters given in Tables 1 through 4, which we call base-case simulation. Mineral dissolution and precipitation rates are a product of the kinetic rate constant and reactive surface area, the magnitudes of which are highly uncertain and cover a wide range of values. Therefore, a number of sensitivity simulations were performed by changing kinetic rate constants.

## **4. Results and Discussion**

### **4.1. Base Case**

Concentrations of aqueous chemical components through the sandstone-shale transect are presented in Figure 2. To track diffusive transport fronts, a non-reactive tracer concentration of 1 was applied initially to the sandstone grid block. Figure 2a shows tracer concentration distribution at different times. The initial pH in the sandstone is 7.34, and that in shale is 6.69. The imposition of a high CO<sub>2</sub> pressure of 201 bar lowers the pH in the sandstone (Figure 2b), and H<sup>+</sup> diffuses from the sandstone to shale. The minimum pH after 10,000 years is located about 3 m into the shale, which is behind the tracer front due to retardation by chemical reactions. The movement of H<sup>+</sup> is consistent with carbonate behavior (Figure 2c). Early in the simulation, the carbonate concentration and pH in the shale are controlled mainly by kerogen-OS decomposition. Later, they are gradually affected by CO<sub>2</sub> diffusion from the sandstone layer. Total iron (Fe<sup>+2</sup> + Fe<sup>+3</sup>) diffuses from the shale to sandstone (Figure 2d) because in the sandstone Fe<sup>+2</sup> is removed

by precipitation of siderite ( $\text{FeCO}_3$ ) and ankerite ( $\text{CaMg}_{0.3}\text{Fe}_{0.7}(\text{CO}_3)_2$ ).  $\text{Ca}^{+2}$  also diffuses from the shale into the sandstone (Figure 2e) due to ankerite precipitation, its behavior being similar to total iron. A significant  $\text{Mg}^{+2}$  concentration buildup occurs only after 10,000 yr at a distance range from 2 to 5 m (Figure 2f).  $\text{Na}^+$  concentration (Figure 2g) increases up to 10,000 yr due to the dissolution of oligoclase ( $\text{CaNa}_4\text{Al}_6\text{Si}_{14}\text{O}_{40}$ ). Simultaneously,  $\text{Na}^+$  diffuses from the sandstone to the shale due to the higher abundance of oligoclase in the former (Table 3). Finally  $\text{Na}^+$  diffusion reverses direction because oligoclase dissolves completely in both rocks and early precipitated low-albite in the shale starts to dissolve and supply  $\text{Na}^+$  to pore fluid. The  $\text{K}^+$  concentration (Figure 2h) also increases until 10,000 yr when K-feldspar disappears due to dissolution. Considerably higher  $\text{K}^+$  concentration occurs in the sandstone due to the higher K-feldspar abundance.  $\text{Al}^{+3}$  and  $\text{SiO}_2(\text{aq})$  concentrations (Figures 2i and 1j) are controlled by the dissolution and precipitation of a number of aluminosilicate minerals. The total sulfur (sulfate and sulfide species) concentration (Figure 2k) is buffered by kerogen-OS dissolution and pyrite precipitation.

We now turn to the dissolution and precipitation of mineral phases along the sandstone-shale transect. The abundances of mineral phases (both primary and secondary) with time are presented in Figure 3. Significant dissolution of calcite occurs in the sandstone due to the lower pH induced by the presence of  $\text{CO}_2$  at high pressure (Figure 3a), as can be seen clearly in Figure 6, which gives a time evolution profile in the sandstone. Slight dissolution and precipitation of calcite occurs in the interior of the shale over time. Oligoclase disappears very rapidly between 1,000 and 10,000 yr (Figure 3b) in both sandstone and shale layers. K-feldspar is similarly destroyed just after 10,000 yr in both layers. Chlorite (Figure 3d) dissolution also occurs in both layers to supply  $\text{Fe}^{+2}$  needed for precipitation of siderite and ankerite. Chlorite disappears in the sandstone just after 1,000 yr. Some chlorite remains in the interior of the shale at 10,000 yr, but no chlorite remains at 100,000 yr. Kaolinite dissolves steadily in both layers (Figure 3e). Na-smectite dissolution occurs mostly in the sandstone and in the shale close to the interface (Figure 3f). Hematite dissolution (Figure 3g) initially occurs in the sandstone to supply  $\text{Fe}^{+2}$  needed for precipitation of siderite and ankerite, and progressively proceeds into the shale interior over time. This behavior is similar to chlorite dissolution. Kerogen-OS



dissolves steadily and constantly in the shale (Figure 3h). Quartz precipitates in the sandstone but remains essentially at equilibrium in the interior of the shale (Figure 3i). Illite (Figure 3j) precipitates due to dissolution of oligoclase and K-feldspar, particularly in the shale close to the interface. Low-albite precipitation occurs at 10,000 years in both layers but most intensively at a depth of 4 m in the shale (Figure 3k). However, low-albite later disappears to supply Na needed for dawsonite precipitation. Pyrite precipitates steadily in the shale due to the release of sulfide by dissolving kerogen-OS (Figure 3l).

The injected CO<sub>2</sub> is immobilized by precipitation of four carbonate minerals: magnesite (MgCO<sub>3</sub>), siderite (FeCO<sub>3</sub>), ankerite (CaMg<sub>0.3</sub>Fe<sub>0.7</sub>(CO<sub>3</sub>)<sub>2</sub>), and dawsonite (NaAlCO<sub>3</sub>(OH)<sub>2</sub>). Minor magnesite forms close to the interface in the shale between 1,000 and 10,000 yr (Figure 3m), but later dissolves completely. Therefore, magnesite is not a stable CO<sub>2</sub> trapping mineral in the modeled environment. Siderite precipitates initially only in the sandstone (Figure 3n), but later gradually forms in the shale due to diffusive transport of CO<sub>2</sub> from the sandstone. The detailed temporal evolution of carbonate minerals in the sandstone can be seen in Figure 6. Significant CO<sub>2</sub> is immobilized by precipitation of ankerite and dawsonite (Figures 3o and 3p). After 100,000 years a maximum of approximately 4% and 6% of volume fraction of ankerite and dawsonite are formed in the sandstone. Calcite dissolves under the high CO<sub>2</sub> pressure conditions, and no dolomite (CaMg(CO<sub>3</sub>)<sub>2</sub>) precipitation is observed. The cumulative CO<sub>2</sub> sequestered in carbonate minerals along the sandstone-shale transect is presented in Figure 4. Precipitation of carbonate minerals initially occurs essentially in the sandstone, and later gradually occurs in the shale due to diffusive transport of CO<sub>2</sub> from the sandstone. The precipitation of carbonate minerals results in decrease of porosity (Figures 5 and 8), which is consistent with CO<sub>2</sub> mineral sequestration shown in Figure 4. A slight increase in porosity can be observed in the interior of the shale (x > 4 m), indicating leaching chemical constituents from the shale.

After 100,000 years, CO<sub>2</sub> mineral sequestration in the sandstone can reach about 90 kg/m<sup>3</sup> of medium (Figure 7), which is very close to the maximum capacity. The CO<sub>2</sub> trapping capacity depends on the primary mineral composition. Precipitation of siderite and ankerite requires Fe<sup>+2</sup> supplied mostly by chlorite (Mg<sub>2.5</sub>Fe<sub>2.5</sub>Al<sub>2</sub>Si<sub>3</sub>O<sub>10</sub>(OH)<sub>8</sub>) and some by dissolution and reduction of hematite (Fe<sub>2</sub>O<sub>3</sub>). Precipitation of dawsonite

requires  $\text{Na}^+$  provided by oligoclase ( $\text{CaNa}_4\text{Al}_6\text{Si}_{14}\text{O}_{40}$ ) dissolution. The initial abundance of chlorite and oligoclase therefore affects the  $\text{CO}_2$  mineral trapping capacity. The sequestration time required depends on the kinetics of mineral dissolution and precipitation. In the next section, we discuss sensitivity of  $\text{CO}_2$  mineral sequestration to kinetic rate constants.

## 4.2. Sensitivity

Mineral dissolution and precipitation rates are a product of the kinetic rate constant and reactive surface area (Eq. 1), the magnitudes of which are highly uncertain and cover a wide range of values. Scaling kinetic rate constants (or reactive surface areas) for all minerals by the same factor is equivalent to scaling the time coordinate. These changes result in reciprocal changes in the time scale. Details on scaling kinetic rates by the same factor are given in Xu et al. (2004)

As shown above, significant  $\text{CO}_2$  is sequestered by dawsonite precipitation. The overall sequestration time required depends strongly on the kinetics of dawsonite precipitation. Dawsonite reaction kinetics is not well understood. In the previous simulation, we simply set the rate constant equal to that of siderite and ankerite ( $k_{25} = 1.2589 \times 10^{-9} \text{ moles m}^{-2}\text{s}^{-1}$  in Table 1). In order to examine the effect of dawsonite precipitation kinetics on sequestration time, two additional simulations were performed by decreasing the rate constant used in the base case by two and three orders of magnitude, respectively. The cumulative  $\text{CO}_2$  mineral sequestration after 100,000 years along the sandstone-shale transect obtained by these sensitivity simulations is presented in Figure 9. At the final time (after 100,000 years), total  $\text{CO}_2$  sequestered in the sandstone decreases slightly with the rate constant. While, the total amount of  $\text{CO}_2$  sequestered in the shale is very close to that in the base case, except that the peak concentration is shifted somewhat towards the sandstone interface. The dawsonite distribution (Figure 10a) after 100,000 years is similar to  $\text{CO}_2$  mineral sequestration. The decreases in dawsonite kinetic rate constant results in very slight decreases in ankerite precipitation in the sandstone, and slight increases in the shale (Figure 10b). The detailed temporal evolutions of  $\text{CO}_2$  sequestration and carbonate mineral abundance are presented in

Figures 11 and 12, respectively. As expected, the lower rate constant results in less dawsonite precipitation. However, the difference decreases with time when compared to the base case. After 100,000 years, the CO<sub>2</sub> mineral sequestration is only slightly lower than the base case. Thus, a decrease in the dawsonite rate constant by two or three orders of magnitude results in a small decrease in the mineral sequestration. The reason for the small effect is because precipitation of dawsonite requires reactants that are provided by the dissolution of the primary aluminosilicate minerals. For example, Na<sup>+</sup> required by dawsonite precipitation comes from dissolution of oligoclase (CaNa<sub>4</sub>Al<sub>6</sub>Si<sub>14</sub>O<sub>40</sub>). In the base case, the dawsonite precipitation rate is limited by the dissolution rate of aluminosilicate minerals even though a higher dawsonite rate constant was used.

#### **4.3. Comparison with field observations**

Few mineralogical descriptions of the alteration of sandstone – shale sequences in the presence of high-pressure CO<sub>2</sub> are available in the literature that would allow comparison with the simulation presented in this paper. Those of interest usually reflect past accumulations of CO<sub>2</sub> associated with magmatic or volcanic activity. An example is that by Moore et al. (this issue), who describe the formation of secondary dawsonite and kaolinite in siltstones of the Permian Supai Formation of the Springerville-St. John CO<sub>2</sub> field on the border between Arizona and New Mexico. They observed secondary dawsonite spatially associated with corroded plagioclase and potassium feldspar, which is consistent with our simulations. Furthermore, their determination that kaolinite formed subsequent to dawsonite deposition following a decline in the CO<sub>2</sub> pressure, is also consistent with our finding that kaolinite is unstable during the precipitation of dawsonite. Authigenic illite appears to persist in the presence of dawsonite, which is also consistent with our modeling results. In contrast, the Supai Formation appears to have been more oxidizing, with a limited capacity to provide Fe<sup>+2</sup> for the stabilization of ankerite.

Another recent paper (Watson et al., 2002) describes mineralogical and groundwater changes caused by magmatic carbon dioxide invading a gas reservoir in a lithic sandstone of the Pretty Hill Formation in the Ladbroke Grove gas field in South Australia. An important feature of this field example is that the mineralogy can be

compared with an adjacent unmodified methane gas reservoir in the same formation. In contrast to those of the Supai Formation of Arizona and New Mexico, the conditions in this high-pressure CO<sub>2</sub> field are such that Fe<sup>+2</sup> is available for the stabilization of siderite and ankerite. In this respect, the Ladbroke Grove field more closely represents the conditions of our simulation. Observed similarities include the destruction of chlorite in the lithic fragments and net corrosion of the feldspars, a reduction in the concentration of calcite, an increase in the concentration of siderite, a significant increase in the quantity of ankerite and a small increase in the quantity of quartz. However, no dawsonite was reported even though an evaluation of the coexisting groundwater indicates that it should have been supersaturated with respect to this carbonate. A substantial increase in the concentration of kaolinite is observed, which is in conflict with our simulation. The porosity of the Ladbroke Grove reservoir also appears to have increased, whereas our simulation shows a decrease. The differences might be explained by the higher CO<sub>2</sub> pressure (201 vs. approximately 150 bar) and the higher Cl<sup>-</sup> and Na<sup>+</sup> concentrations of the simulation.

Other field evidence supports that magmatic CO<sub>2</sub> can also lead to the formation of dawsonite in arenaceous sedimentary formations, notably in the Bowen, Gunnedah and Sydney Basins of New South Wales (Baker et al., 1995), and the Denison Trough of east-central Queensland (Baker, 1991; Baker and Caritat, 1992). Dawsonite and kaolinite in these sedimentary accumulations appear to have been produced at the expense of detrital feldspars, in general agreement with the observations of Moore et al. (this issue). But it should be noted that feldspar destruction is incomplete, and on occasion, dawsonite is found in juxtaposition with unaltered feldspar (Loughnan and Goldbery, 1972). The field evidence is therefore suggestive of slow feldspar corrosion rates if not the eventual stabilization of feldspars. In these sedimentary formations, the occurrence of dawsonite is unrelated to the preceding precipitation or dissolution of diagenetic calcite, siderite and ankerite, which is attributed to early diagenesis and subsequent organic maturation (Baker, 1991).

Carbonate paragenesis in sedimentary formations invaded by magmatic CO<sub>2</sub> can vary in degree and complexity. The mineralogy, burial history, diagenesis, organic maturation, temperature and connate water salinity all play a role in addition to the timing

and extent of magmatic CO<sub>2</sub> involvement. Thus it is hardly surprising that agreement between the present simulations and field observations is not perfect in all respects.

## 5. Summary and Conclusions

A reactive geochemical transport model for a sandstone-shale system under high CO<sub>2</sub> pressure conditions has been developed. The model has been used to analyze mass transfer of aqueous chemical components, the alteration pattern of minerals, sequestration of CO<sub>2</sub> by secondary carbonates, and changes of porosity for a Gulf Coast aquifer.

CO<sub>2</sub> diffuses from the sandstone (where CO<sub>2</sub> is initially injected), lowering pH. Fe<sup>+2</sup> from chlorite dissolution and Ca<sup>+2</sup> from oligoclase dissolution diffuses from the shale to sandstone to supply reactants needed for precipitation of siderite and ankerite. but later reverses direction. Na<sup>+</sup> in contrast to Ca<sup>+2</sup>, initially diffuses from the shale to sandstone, but later reverses direction. Total iron behaves similarly to Ca<sup>+2</sup>, due to significant precipitation of ankerite in the sandstone. Initially, Na<sup>+</sup> diffuses from the sandstone to shale due to higher dissolution rate of oligoclase in the sandstone than in the shale. Finally Na<sup>+</sup> reverses diffusion direction from the shale to sandstone because oligoclase dissolved completely in both layers and early precipitated low-albite in the shale starts to dissolve to supply Na<sup>+</sup> for dawsonite precipitation

Most CO<sub>2</sub> sequestration occurs in the sandstone. The major CO<sub>2</sub> trapping minerals are dawsonite and ankerite. The CO<sub>2</sub> mineral-trapping capacity after 100,000 years reaches 90 kg/m<sup>3</sup> of medium. Precipitation of secondary carbonates results in decreased porosity. Leaching of chemical constituents from the interior of the shale causes slightly increased porosity. The CO<sub>2</sub> trapping capacity depends on its primary mineral composition. Precipitation of siderite and ankerite requires Fe<sup>+2</sup> supplied mainly by chlorite and by some hematite dissolution. Precipitation of dawsonite requires Na<sup>+</sup> provided by oligoclase dissolution. Therefore, the initial abundance of chlorite and oligoclase affects CO<sub>2</sub> mineral trapping capacity.

The sequestration time required depends on the rates of mineral dissolution and precipitation, which are products of the kinetic rate constant and reactive surface area.

Scaling kinetic rates for all minerals by the same factor is equivalent to scaling the time coordinate. Such changes result in reciprocal changes to the time scale. Significant CO<sub>2</sub> is sequestered by dawsonite precipitation. However, dawsonite reaction kinetics are not well understood. The sensitivity regarding dawsonite precipitation rate was examined. Decreases in the rate constant by two and three orders of magnitude result in small decreases in the CO<sub>2</sub> sequestration, because precipitation of dawsonite requires reactants whose availability is controlled by the dissolution of aluminosilicate minerals. In the base case, the dawsonite precipitation rate is limited by the dissolution rate of aluminosilicate minerals even though a higher dawsonite rate constant was used. The overall rate is the lowest value among the participating minerals.

Limited information currently available describing the mineralogy of natural high-pressure CO<sub>2</sub> gas reservoirs is also generally consistent with our simulation.

The model investigated here assumes perfect mixing throughout the sand layer. Future work should examine the effect of regional groundwater flow, including the possibility that groundwater flow in the sandstone is sufficiently slow, so that chemical gradients may develop within the sandstone as a function of distance from the interface with the shale.

The range of problems concerning the interaction of water-CO<sub>2</sub>-rock is very broad. The present simulation results are specific to the conditions and parameters considered. The “numerical experiments” give a detailed understanding of the dynamic evolution of a sandstone-shale geochemical system.

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**Table 1.** List of kinetic rate parameters used in Eqs. (1) and (2) for minerals considered in the present simulations (The rate constant  $k_{25}$  is for far from equilibrium conditions).

Mineral	$k_{25}$ (moles $\text{m}^{-2}\text{s}^{-1}$ )	$E_a$ (KJ/mol)	n	Reference	Surface area ( $\text{cm}^2/\text{g}$ )
calcite	Equilibrium				
quartz	$1.26 \times 10^{-14}$	87.50	0	Tester et al. (1994)	9.8
K-feldspar	$1.00 \times 10^{-12}$	57.78	0	Blum and Stillings (1995)	9.8
	$3.55 \times 10^{-10}$	51.83	0.4	Blum and Stillings (1995)	9.8
kaolinite	$1.00 \times 10^{-13}$	62.76	0	Nagy (1995)	151.6
	$4.37 \times 10^{-12}$	62.76	0.17	Nagy (1995)	151.6
magnesite	$4.47 \times 10^{-10}$	62.76	0	Chou et al. (1989)	9.8
	$4.37 \times 10^{-5}$	18.98	1.0	Chou et al. (1989)	9.8
siderite	$1.26 \times 10^{-9}$	62.76	0	Steefel (2001)	9.8
	$1.02 \times 10^{-3}$	20.90	0.9	Gautelier et al. (1999)	9.8
dolomite	$1.26 \times 10^{-9}$	62.76	0	Set to siderite	9.8
	$1.02 \times 10^{-3}$	20.90	0.9	Set to siderite	9.8
ankerite	$1.26 \times 10^{-9}$	62.76	0	Set to siderite	9.8
	$1.02 \times 10^{-3}$	20.90	0.9	Set to siderite	9.8
dawsonite	$1.26 \times 10^{-9}$	62.76	0	Set to siderite	9.8
	$1.02 \times 10^{-3}$	20.90	0.9	Set to siderite	9.8
kerogen-OS	$1.00 \times 10^{-13}$	0.0	0.0	Assumed	10
oligoclase	$1.00 \times 10^{-12}$	57.78	0	Set to K-feldspar	10
	$3.55 \times 10^{-10}$	51.83	0.4	Set to K-feldspar	10
albite-low	$1.00 \times 10^{-12}$	67.83	0	Blum and Stillings (1995)	9.8
	$2.04 \times 10^{-10}$	59.77	0.5	Blum and Stillings (1995)	98
Na-smectite	$1.00 \times 10^{-13}$	62.76	0	Set to kaolinite	151.6
	$4.37 \times 10^{-12}$	62.76	0.17	Set to kaolinite	151.6
Ca-smectite	$1.00 \times 10^{-13}$	62.76	0	Set to kaolinite	151.6
	$4.37 \times 10^{-12}$	62.76	0.17	Set to kaolinite	151.6
illite	$1.00 \times 10^{-13}$	62.76	0	Set to kaolinite	151.6
	$4.37 \times 10^{-12}$	62.76	0.17	Set to kaolinite	151.6
pyrite	$4.00 \times 10^{-11}$	62.76	0	Ague and Brimhall (1989)	12.9
hematite	$4.00 \times 10^{-11}$	62.76	0	Set to pyrite	12.9
chlorite	$2.51 \times 10^{-12}$	62.76	0	Malmstrom et al. (1996)	9.8

**Table 2.** Hydrogeologic parameters for sandstone and shale layers.

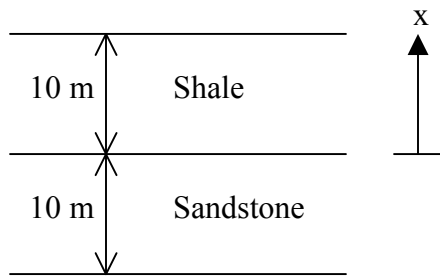
Parameters	Sandstone	Shale
Permeability (m <sup>2</sup> )	10 <sup>-13</sup>	10 <sup>-18</sup>
Porosity	0.3	0.1
Tortuosity	0.3	0.1
Compressibility (Pa <sup>-1</sup> )	1x10 <sup>-8</sup>	1x10 <sup>-8</sup>
Diffusivity (m <sup>2</sup> /s)	1x10 <sup>-9</sup>	1x10 <sup>-9</sup>
Relative permeability		
Liquid (van Genuchten, 1980):  $k_{rl} = \sqrt{S^*} \left\{ 1 - \left( 1 - [S^*]^{1/m} \right)^m \right\}^2$ $S_{lr}$ : irreducible water saturation m: exponent	$S^* = (S_l - S_{lr}) / (1 - S_{lr})$  $S_{lr} = 0.00$ $m = 0.457$	$S_{lr} = 0.00$ $m = 0.457$
Gas (Corey, 1954):		
$k_{rg} = (1 - \hat{S})^2 (1 - \hat{S}^2)$  $S_{gr}$ : irreducible gas saturation	$\hat{S} = \frac{(S_l - S_{lr})}{(S_l - S_{lr} - S_{gr})}$  $S_{gr} = 0.05$	$S_{gr} = 0.05$
Capillary pressure		
van Genuchten (1980) $P_{cap} = -P_0 \left( [S^*]^{-1/m} - 1 \right)^{1-m}$ $S_{lr}$ : irreducible water saturation m: exponent $P_0$ : strength coefficient	$S^* = (S_l - S_{lr}) / (1 - S_{lr})$  $S_{lr} = 0.00$ $m = 0.457$ $P_0 = 19.61 \text{ kPa}$	$S_{lr} = 0.00$ $m = 0.457$ $P_0 = 6.2 \text{ MPa}$

**Table 3.** List of initial mineral volume fractions and secondary mineral phases for sandstone and shale layers (dolomite and Ca-smectite were included in the list of possible secondary mineral phases the simulations but they were not formed).

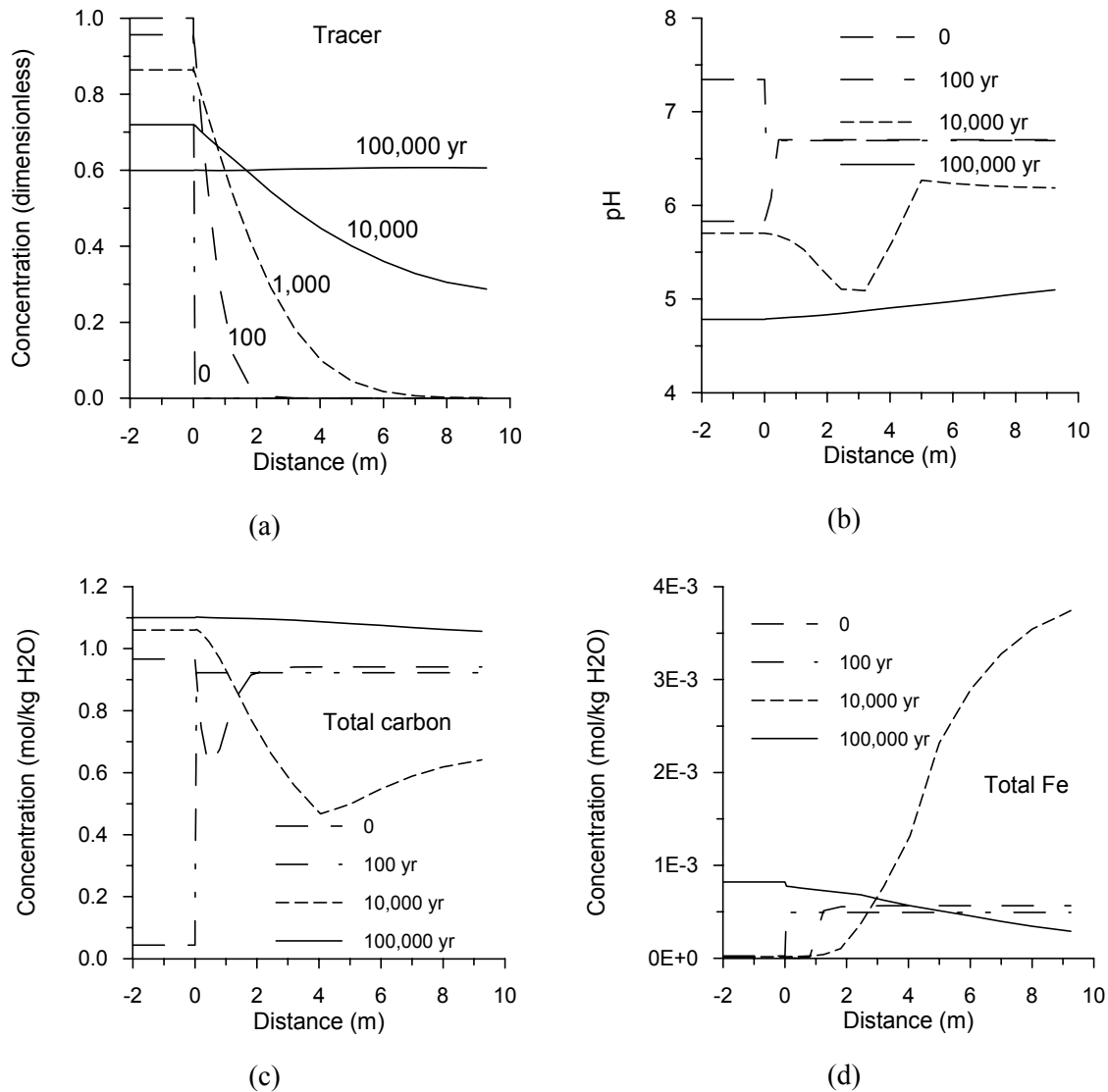
Mineral	Chemical composition	Vol.% of solid rock		Vol.% of medium	
		Sandstone	Shale	Sandstone	Shale
<b>Primary:</b>					
quartz	SiO <sub>2</sub>	58	19.22	40.6	17.3
kaolinite	Al <sub>2</sub> Si <sub>2</sub> O <sub>5</sub> (OH) <sub>4</sub>	2.02	4.37	1.41	3.95
calcite	CaCO <sub>3</sub>	1.93	10.9	1.35	9.81
illite	K <sub>0.6</sub> Mg <sub>0.25</sub> Al <sub>1.8</sub> (Al <sub>0.5</sub> Si <sub>3.5</sub> O <sub>10</sub> )(OH) <sub>2</sub>	1.0	28.14	0.7	25.33
kerogen-OS	C <sub>64</sub> H <sub>102</sub> O <sub>40</sub> S <sub>10</sub>	0.0	2.0	0.0	1.8
oligoclase	CaNa <sub>4</sub> Al <sub>6</sub> Si <sub>14</sub> O <sub>40</sub>	19.8	5.28	13.86	4.75
K-feldspar	KAlSi <sub>3</sub> O <sub>8</sub>	8.2	4.74	5.74	4.27
Na-smectite	Na <sub>0.290</sub> Mg <sub>0.26</sub> Al <sub>1.77</sub> Si <sub>3.97</sub> O <sub>10</sub> (OH) <sub>2</sub>	4	23.0	2.8	20.7
chlorite	Mg <sub>2.5</sub> Fe <sub>2.5</sub> Al <sub>2</sub> Si <sub>3</sub> O <sub>10</sub> (OH) <sub>8</sub>	4.55	2.35	3.19	2.12
hematite	Fe <sub>2</sub> O <sub>3</sub>	0.5	0.0	0.35	0.0
porosity	----	----	----	30	10
<b>Secondary:</b>					
anhydrite	CaSO <sub>4</sub>				
magnesite	MgCO <sub>3</sub>				
low-albite	NaAlSi <sub>3</sub> O <sub>8</sub>				
siderite	FeCO <sub>3</sub>				
pyrite	FeS <sub>2</sub>				
ankerite	CaMg <sub>0.3</sub> Fe <sub>0.7</sub> (CO <sub>3</sub> ) <sub>2</sub>				
dawsonite	NaAlCO <sub>3</sub> (OH) <sub>2</sub>				
alunite	KAl <sub>3</sub> (OH) <sub>6</sub> (SO <sub>4</sub> ) <sub>2</sub>				

**Table 4.** Initial total dissolved component concentrations (mol/kg H<sub>2</sub>O) for reactive transport simulations in the sandstone-shale system. (Iron is the sum of Fe<sup>+2</sup>, Fe<sup>+3</sup> and their related complexes. Carbon is the sum of CO<sub>2</sub>(aq), CH<sub>4</sub>(aq), and their related species such as HCO<sub>3</sub><sup>-</sup> and acetic acid(aq). Sulfur is the sum of sulfate and sulfide species)

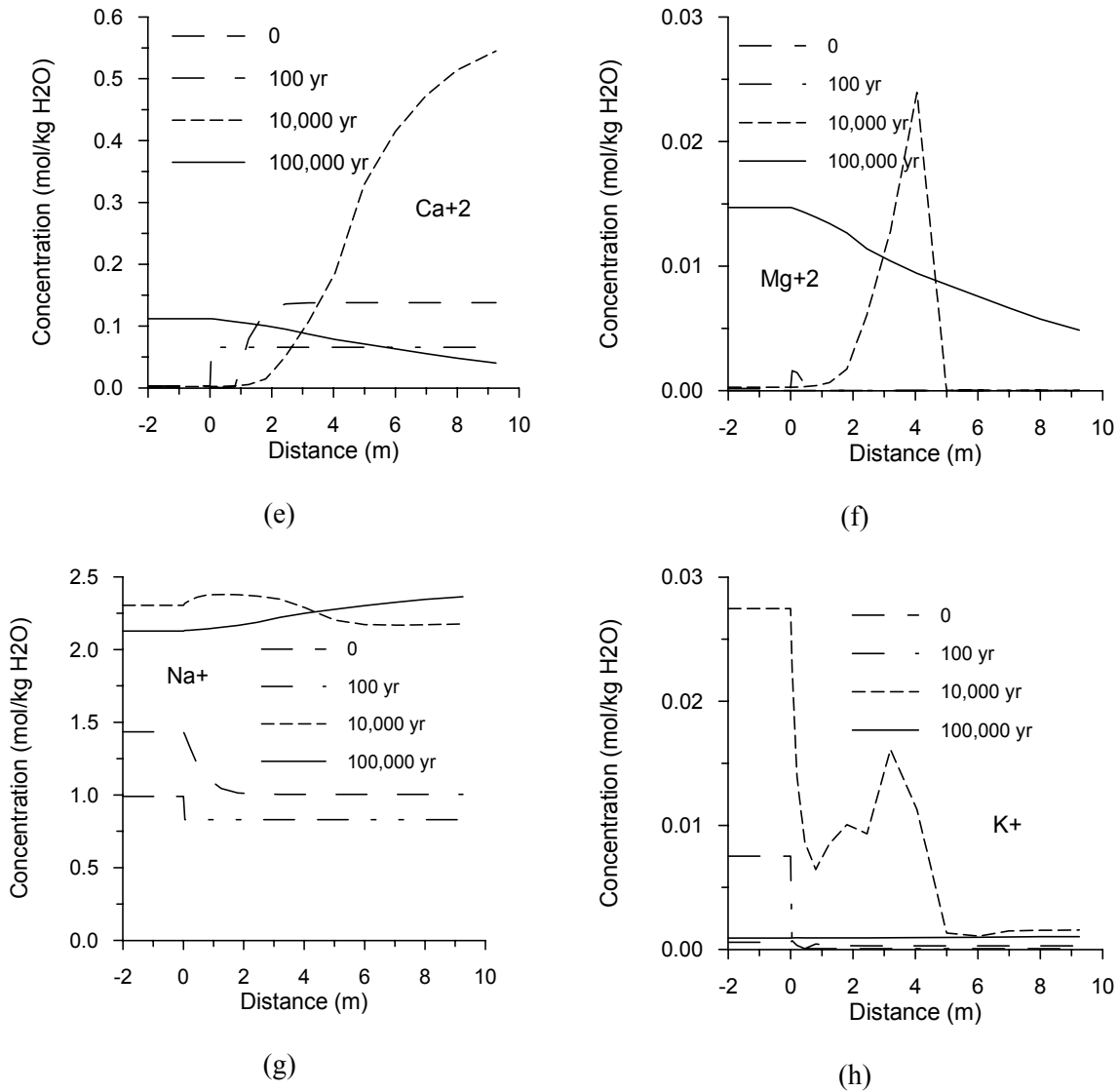
Component	Sandstone	Shale
Ca <sup>+2</sup>	3.23 x10 <sup>-3</sup>	6.57 x10 <sup>-2</sup>
Mg <sup>+2</sup>	1.53 x10 <sup>-7</sup>	6.47 x10 <sup>-7</sup>
Na <sup>+</sup>	0.99	0.83
K <sup>+</sup>	7.52 x10 <sup>-3</sup>	5.6 x10 <sup>-5</sup>
Iron	2.42 x10 <sup>-5</sup>	4.92 x10 <sup>-4</sup>
SiO <sub>2</sub> (aq)	7.26 x10 <sup>-4</sup>	5.89 x10 <sup>-4</sup>
Carbon	4.32 x10 <sup>-2</sup>	0.92
Sulfur	1.32 x10 <sup>-9</sup>	9.72 x10 <sup>-7</sup>
Al <sup>+3</sup>	2.66 x10 <sup>-8</sup>	5.41 x10 <sup>-8</sup>
Cl <sup>-</sup>	1.0	1.0
pH	7.34	6.69
Temperature	75°C	75°C



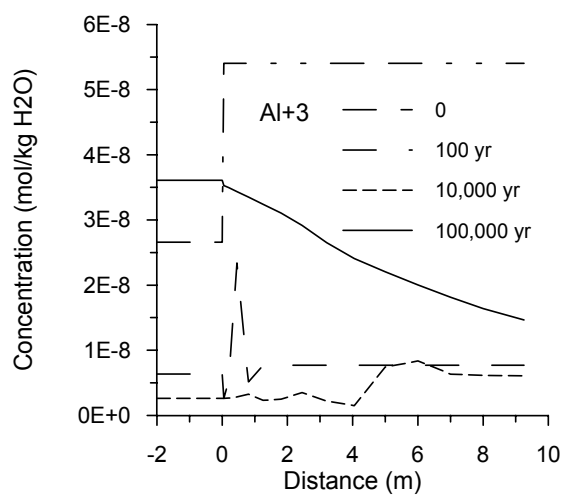
**Figure 1.** Simplified conceptual model for a sandstone-shale system.



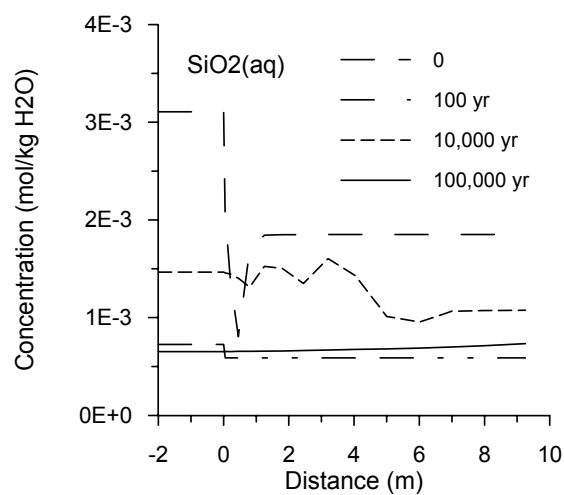
**Figure 2.** Concentrations of aqueous chemical components and pH along the sandstone-shale transect ( $x = 0$  is the interface between sandstone and shale layers. Only two meters of the sandstone layer is shown in the figures where  $x < 0$ ). (a) A non-reactive tracer of unit concentration was applied in the sandstone grid block to track diffusive transport fronts; (b) The initial pH in sandstone is 7.34, and that in shale is 6.69. The imposition of the high CO<sub>2</sub> pressure decreases pH; (c) At initial times, the carbonate concentration and pH in the shale are mainly controlled by kerogen-OS decomposition, and later they are gradually affected by CO<sub>2</sub> diffusion from the sandstone layer; (d) Total iron diffuses from the shale to sandstone, because in the sandstone Fe is consumed by precipitation of siderite (FeCO<sub>3</sub>) and ankerite (CaMg<sub>0.3</sub>Fe<sub>0.7</sub>(CO<sub>3</sub>)<sub>2</sub>).



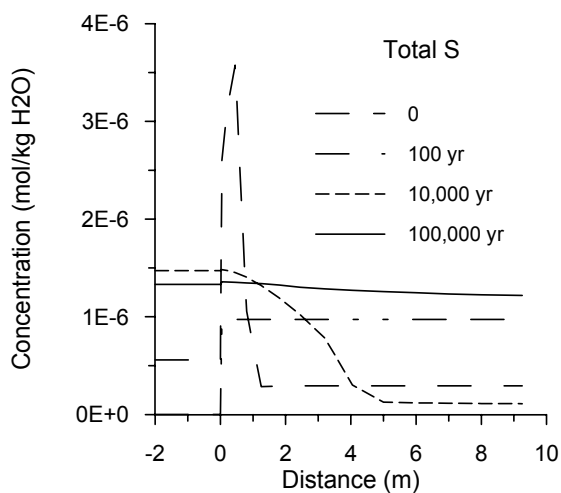
**Figure 2. (Continued).** (e) Ca<sup>2+</sup> diffuses from the shale into the sandstone due to ankerite precipitation; (f) Significant Mg<sup>2+</sup> concentration occurs only after 10,000 yr at a distance into the shale from 2 to 5 m; (g) Na<sup>+</sup> concentration increases until 10,000 yr due to dissolution of oligoclase (CaNa<sub>4</sub>Al<sub>6</sub>Si<sub>14</sub>O<sub>40</sub>), while consequently, Na<sup>+</sup> diffuses from the sandstone to the shale due to a higher abundance of oligoclase in the sandstone than in the shale. Finally Na<sup>+</sup> diffusion reverses direction from the shale to the sandstone, because oligoclase has dissolved completely in both layers and early precipitated low-albite in the shale starts to dissolve to supply Na<sup>+</sup>; (h) K<sup>+</sup> concentration increases until 10,000 yr when K-feldspar disappears due to dissolution. A considerably higher K<sup>+</sup> concentration occurs in the sandstone due to the higher K-feldspar abundance.



(i)



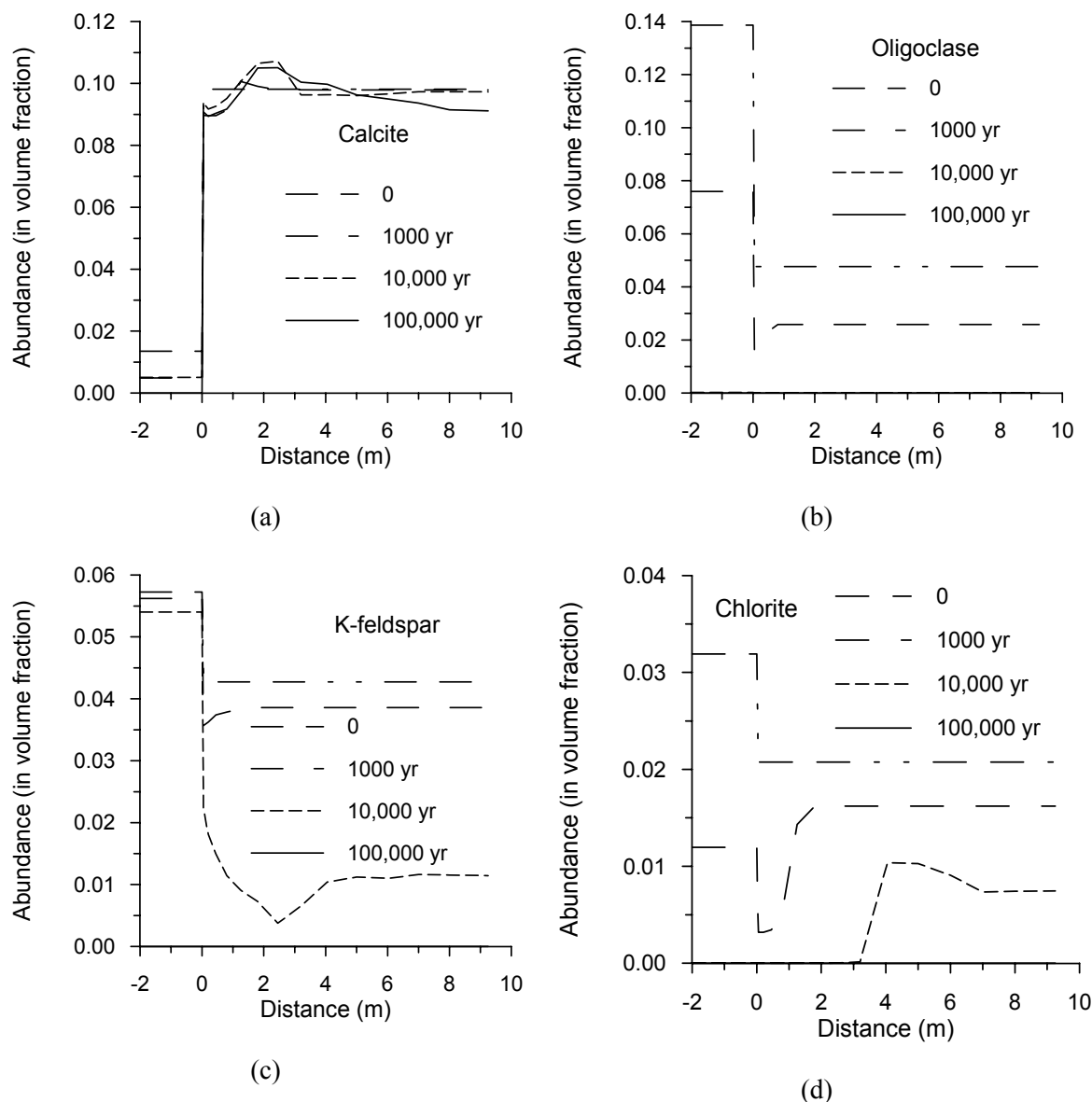
(j)



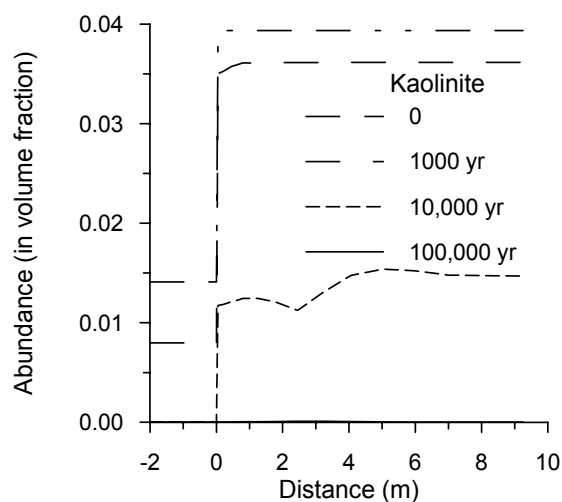
(k)

**Figure 2.** (Continued). (i and j)  $\text{Al}^{+3}$  and  $\text{SiO}_2(\text{aq})$  concentrations are controlled by the dissolution and precipitation of a number of aluminosilicate minerals; (k) Total sulfur concentration is buffered by kerogen-OS dissolution and pyrite precipitation.

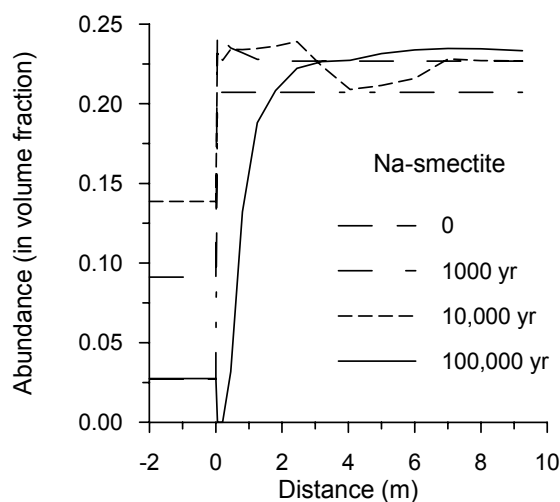




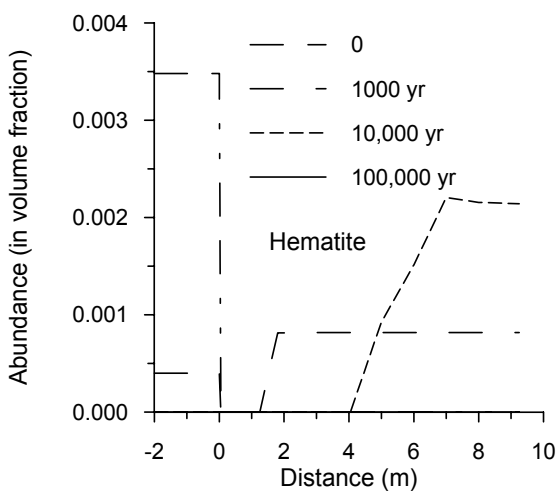
**Figure 3.** Mineral abundances (in volume dimensionless fraction) along the sandstone-shale transect. (a) Significant dissolution of calcite occurs in the sandstone due to lower pH in the presence of high CO<sub>2</sub> pressure. Slight dissolution and precipitation of calcite occurs in the interior of the shale; (b) Oligoclase disappears very rapidly between 1,000 and 10,000 yr in both sandstone and shale layers; (c) K-feldspar is destroyed just after 10,000 yr in both layers; (d) Chlorite dissolution also occurs in both layers, it disappears in the sandstone just after 1,000 yr. Some chlorite remains in the interior of the shale at 10,000 yr, but all chlorite has disappeared by 100,000 yr.



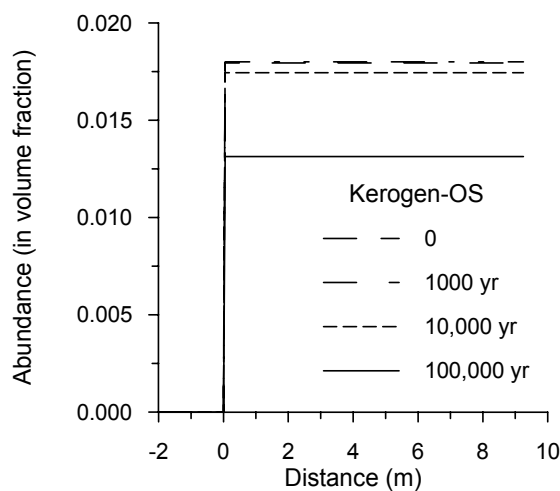
(e)



(f)

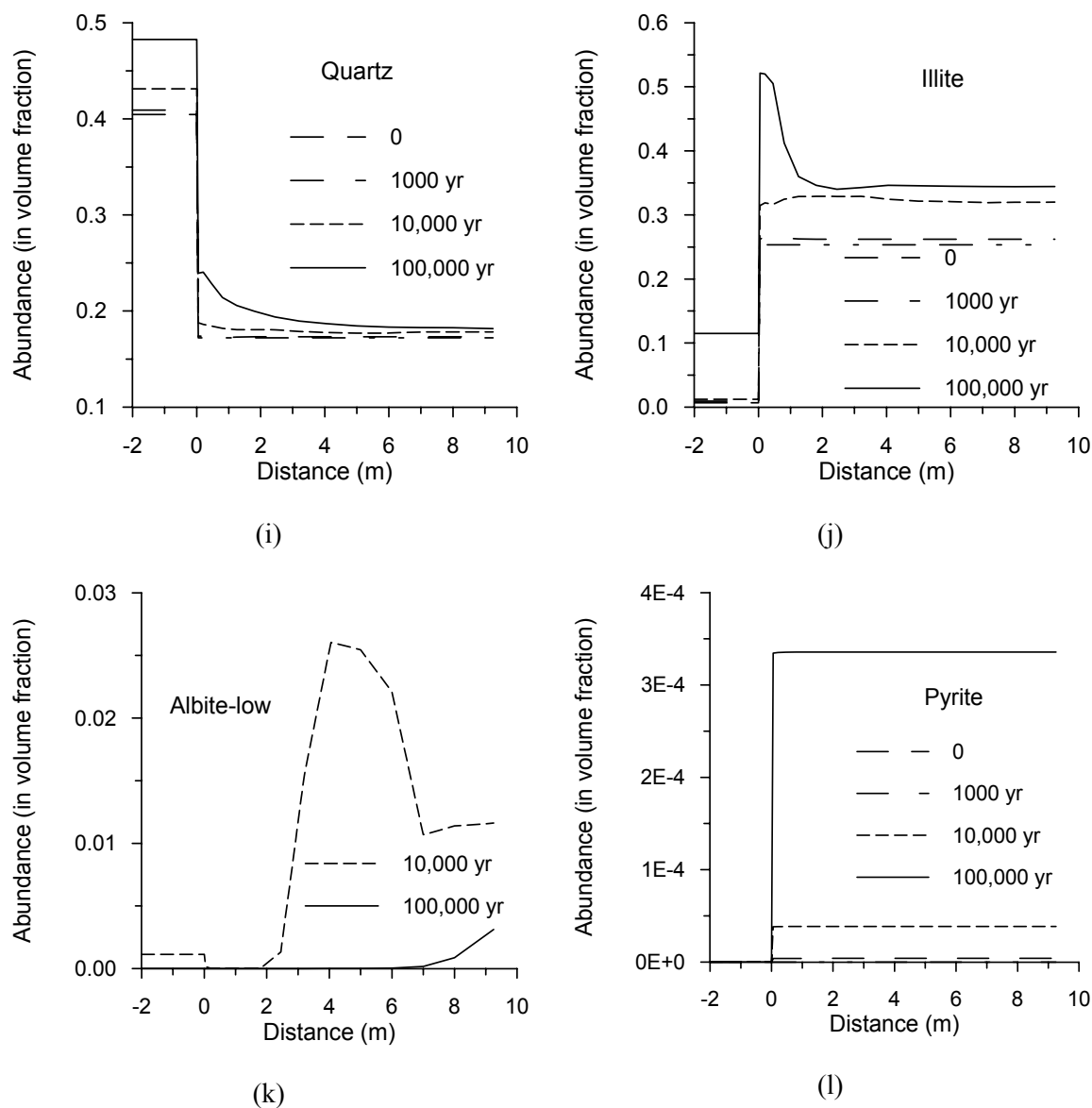


(g)

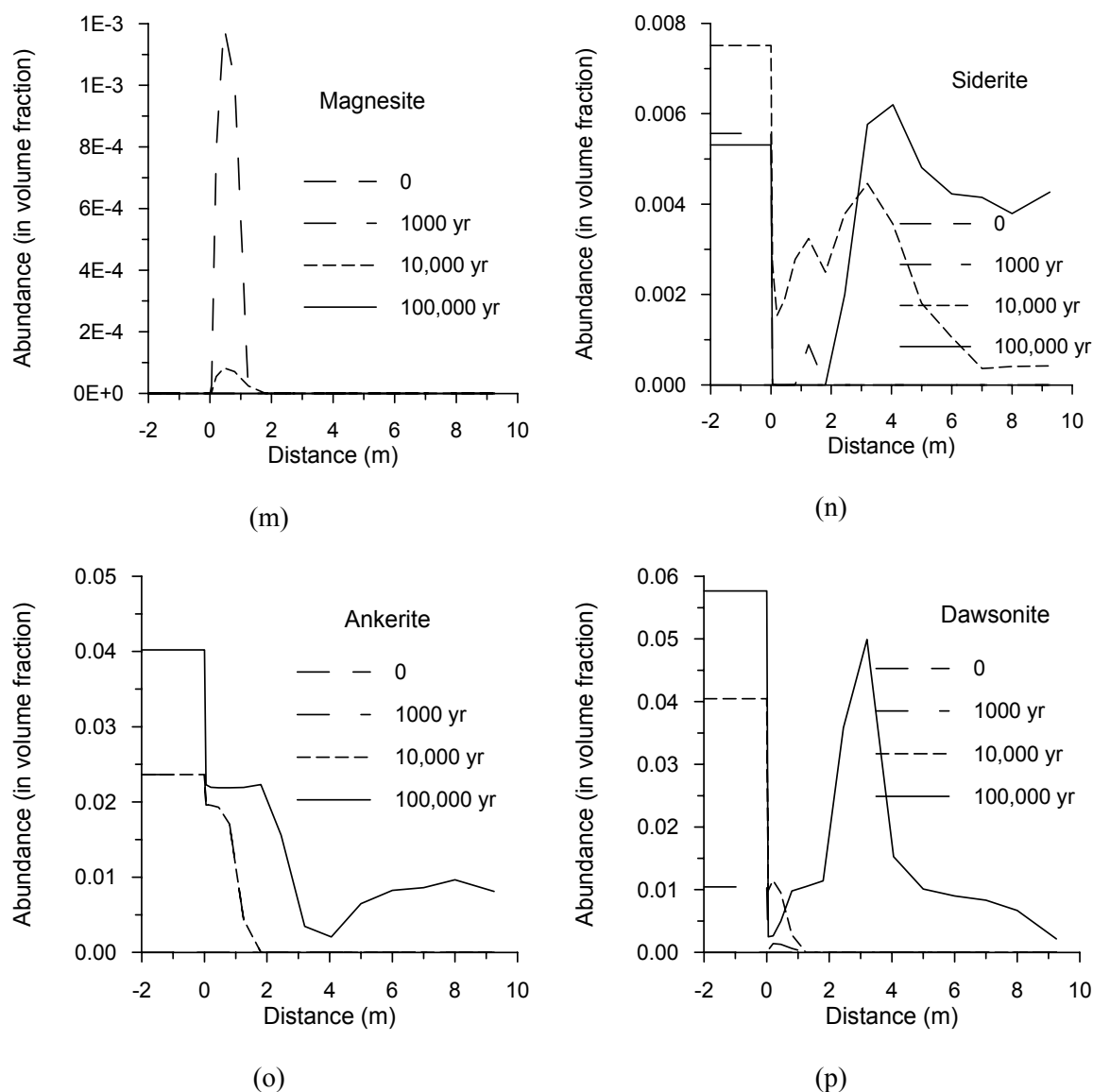


(h)

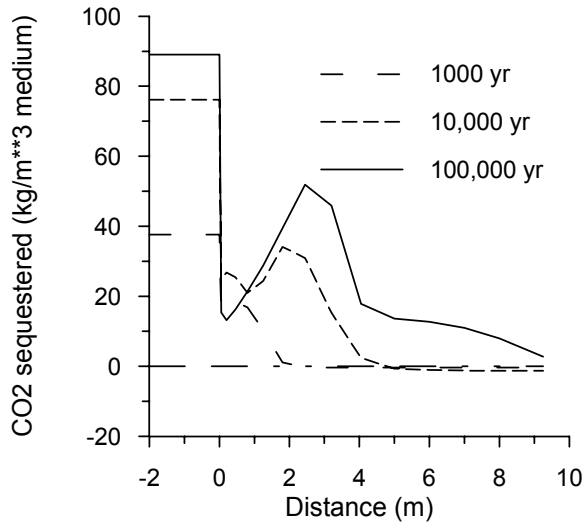
**Figure 3.** (Continued). (e) Kaolinite dissolves steadily in both layers; (f) Na-smectite dissolution occurs mostly in the sandstone and in the shale close to the interface; (g) Hematite dissolution initially occurs in the sandstone, but later precipitates into the shale interior; (h) Kerogen-OS dissolves steadily and uniformly throughout the shale.



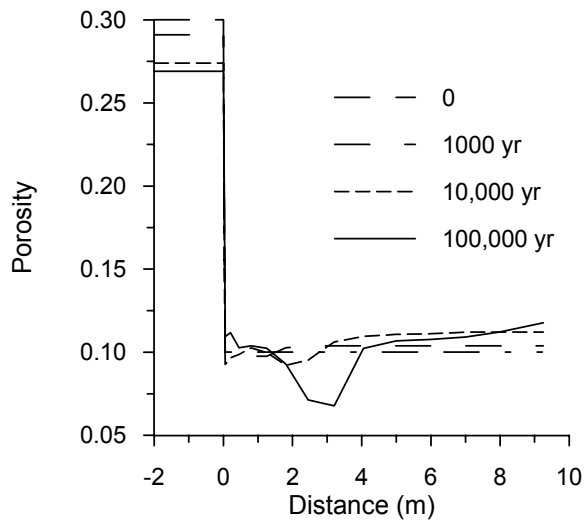
**Figure 3.** (Continued). (i) Quartz precipitates in the sandstone but remains essentially at equilibrium in the interior of the shale; (j) Illite precipitates due to dissolution of K-feldspar, particularly in the shale close to the sandstone interface; (k) Low-albite precipitation occurs at 10,000 yr in both layers with a maximum concentration at  $x = 4$  m, but later dissolves; (l) Pyrite precipitates steadily in the shale due to the release of sulfide by dissolving kerogen-OS.



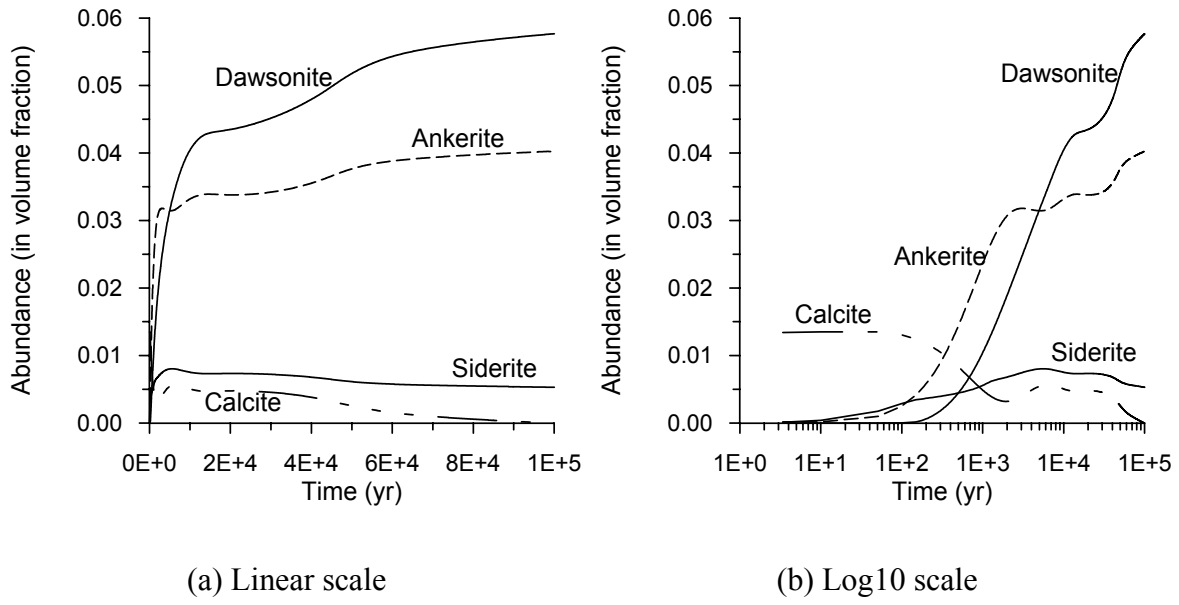
**Figure 3.** (Continued). (m) Minor magnesite forms close to the interface in the shale between 1,000 and 10,000 yr, but later dissolves completely; (n) Siderite precipitation initially occurs only in the sandstone, but later occurs in the shale due to diffusive transport of  $\text{CO}_2$  from the sandstone; (o and p) Significant  $\text{CO}_2$  is respectively immobilized by precipitation of ankerite and dawsonite. After 100,000 years a maximum of approximately 4% and 6% of volume fraction respectively of ankerite and dawsonite are formed in the sandstone.



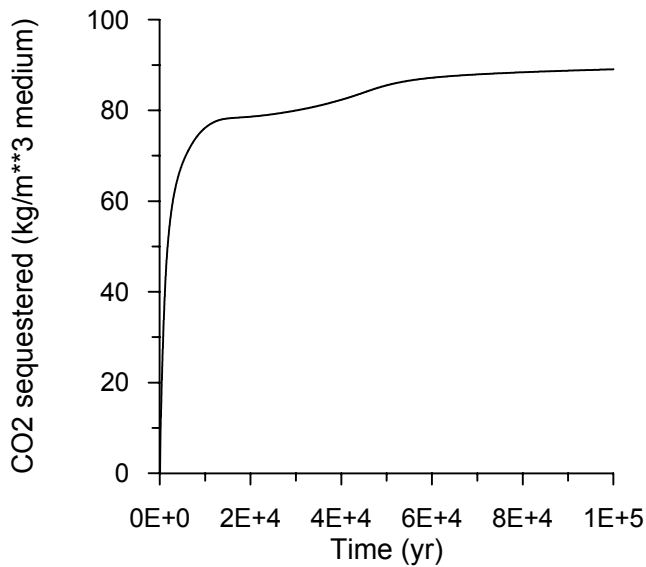
**Figure 4.** Cumulative CO<sub>2</sub> sequestered by carbonate mineral precipitation along the sandstone-shale transect.



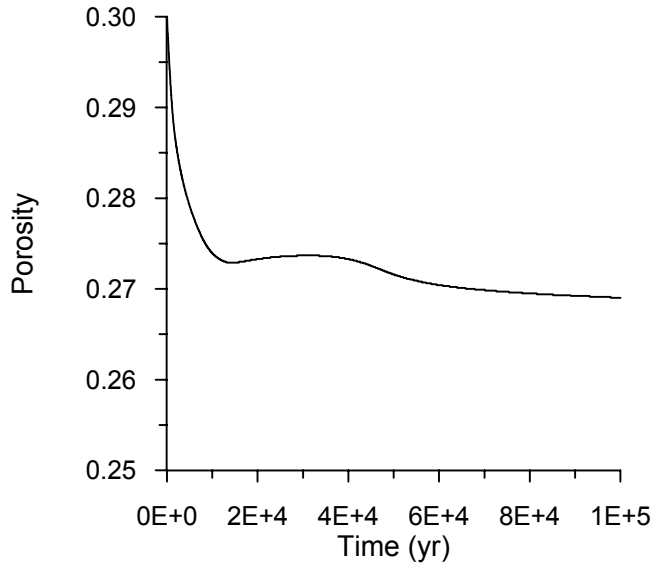
**Figure 5.** Porosity distribution along the sandstone-shale transect. Precipitation of carbonate minerals results in a decrease of porosity, which is consistent with CO<sub>2</sub> mineral sequestration shown in Figure 4. A slight increase in porosity can be observed in the interior of the shale, indicating the leaching of chemical constituents.



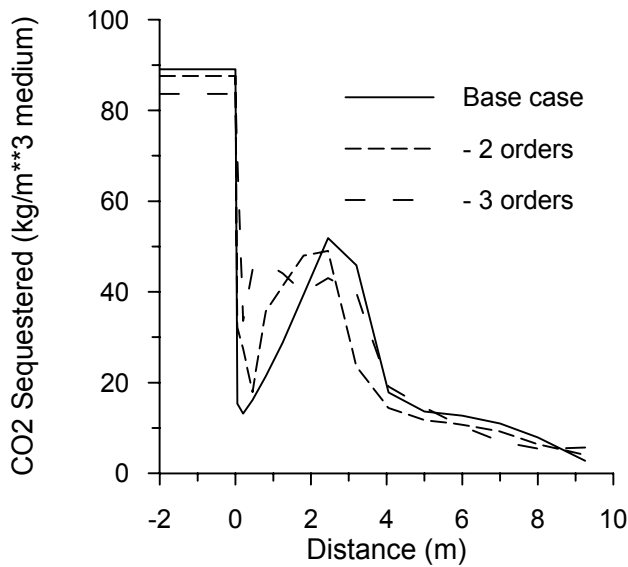
**Figure 6.** Abundances of carbonate minerals over time in the sandstone. Some  $\text{CO}_2$  is immobilized by precipitation of siderite, but more significant by precipitation of ankerite and dawsonite. Precipitation of carbonate minerals occurs primarily before 10,000 yr (a). To emphasize the evolution at initial times, we use a log10 scale for time (b).



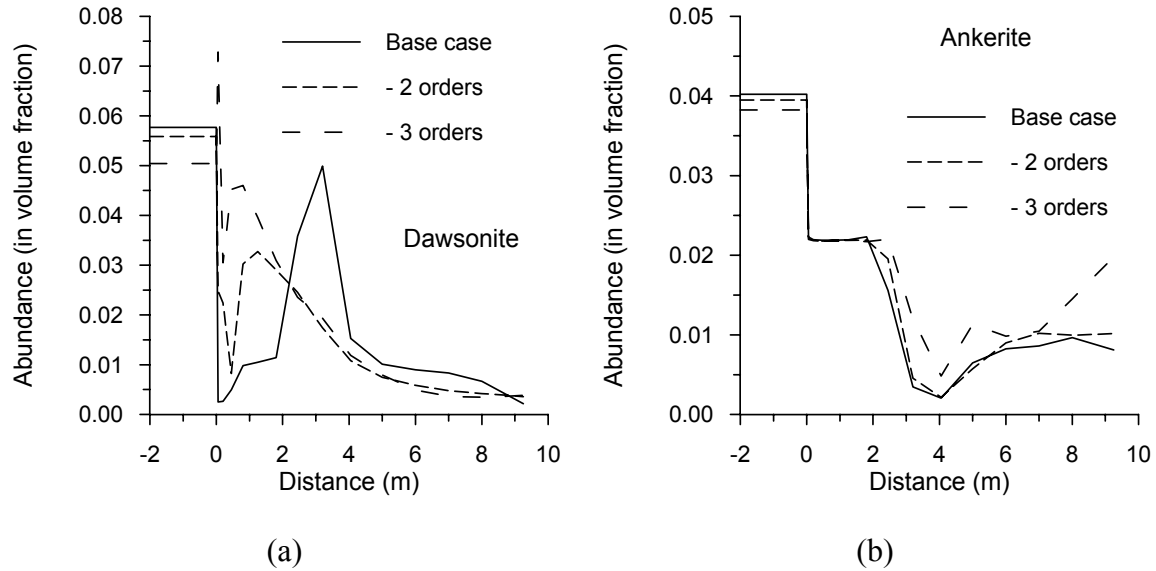
**Figure 7.** Cumulative  $\text{CO}_2$  mineral sequestration over time in the sandstone. Most carbonate minerals precipitate before 10,000 yr consistent with Figure 6.



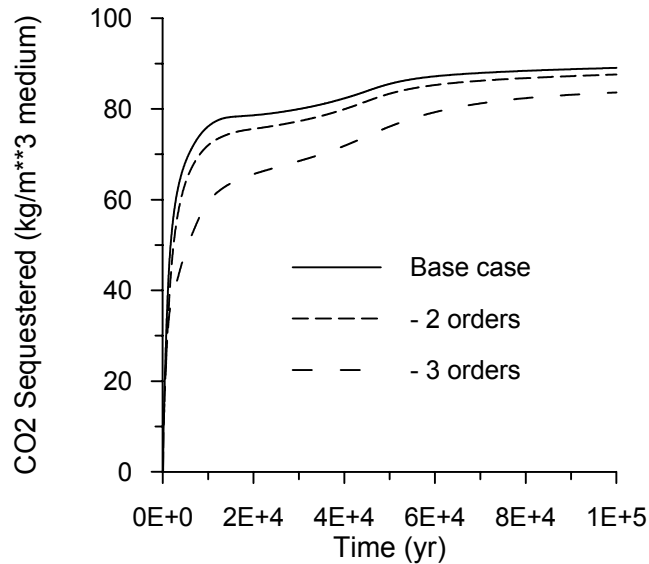
**Figure 8.** Porosity vs. time in the sandstone. Precipitation of carbonate minerals results in a decrease in porosity, which is consistent with CO<sub>2</sub> mineral sequestration shown in Figure 7.



**Figure 9.** Cumulative CO<sub>2</sub> mineral sequestration after 100,000 years along the sandstone-shale transect obtained by decreasing the dawsonite kinetic rate constant. The total CO<sub>2</sub> sequestered in the sandstone decreases slightly with the rate constant. The total amount of CO<sub>2</sub> sequestered in the shale is very close to the base case except that the peak concentration is located closer to the sandstone interface.

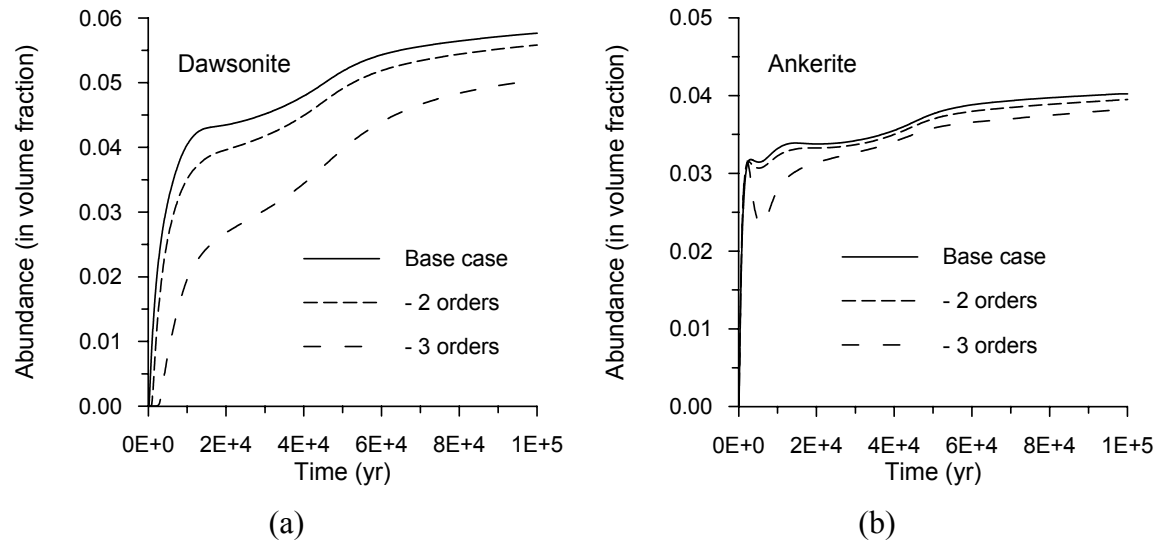


**Figure 10.** Abundance (in volume fraction) of dawsonite and ankerite along the sandstone-shale transect obtained by decreasing the dawsonite kinetic rate constant by two and three orders of magnitude from the base value ( $k_{25} = 1.2589 \times 10^{-9}$  moles  $\text{m}^{-2}\text{s}^{-1}$  in Table 1).



**Figure 11.** Cumulative  $\text{CO}_2$  mineral sequestration vs. time in the sandstone layer obtained by decreasing dawsonite kinetic rate constant.





**Figure 12.** Mineral abundance (in volume fraction) vs. time in the sandstone layer obtained by decreasing dawsonite kinetic rate constant.